Pair correlation functions of simple solutes in a Lennard-Jones solvent*

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Abstract:

We have calculated the pair correlation functions for several binary mixtures composed of simple solutes in a Lennard-Jones solvent. In particular, we have studied the solute-solute pair correlation functions and their dependence on the total density, the solvent Lennard-Jones parameters and on the solute-solute energy parameter. All the results were obtained from solving the Percus-Yevick equations, as well as from Monte Carlo simulations. The relevance of these results to the problem of hydrophobic interactions is also discussed.

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1. <u>Introduction</u>

In the course of studying the underlying molecular origins of the hydrophobic interaction^{1,2}, one of the authors (ABN) examined the potential of mean force (*PMF*) in a one dimensional system composed of a hard-rod solute in two types of solvents. The first was a simple solvent consisting of particles interacting via a square-well potential, and the second was a water-like solvent consisting of particles interacting via hydrogen-bond-like potential functions. ³⁻⁵

The two solvents showed very different behavior in their pure states; one behaved "normally" while the second exhibited water-like behavior. Interestingly, the solubility and the *PMF* of a hard-rod (*HR*) solute in the two solvents could be made very similar in magnitude by adjusting the strength of the solvent-solvent interaction. It was therefore suspected that the strength of the so-called hydrophobic interaction (i.e., the *PMF* between two simple solutes in water) is not a result of the peculiarities of the structure of water but a result of the strength of the solvent-solvent interaction.

To test this conjecture, we have carried out a series of calculations of the pair correlation function (*PCF*) of a simple solute in a Lennard-Jones (*LJ*) solvent. We have examined the dependence of the *PCF* on both the strength of the intermolecular interaction as well as the size of the solvent particles. In the following section, we describe very briefly the methods used to calculate the *PCF*. A sample of results is presented in section 3, and some conclusions on the relevance of these results to the problem of hydrophobic interactions are discussed in section 4.

2. <u>Methods of calculating the pair correlation function</u>

2.1 <u>Numerical solution to the Percus-Yevick equations</u>

All calculations were done for binary mixtures. The solvent *B* consisted of particles interacting through pair potentials of the form

$$U_{BB}(R) = 4\varepsilon_{BB} \left[\left(\frac{\sigma_{BB}}{R} \right)^{12} - \left(\frac{\sigma_{BB}}{R} \right)^{6} \right]$$
(2.1)

where ε represents the strength of the inter particle attraction and σ represents the particle diameter.

The solute A was treated as either hard sphere particles with interaction

$$U_{AA}(R) = \begin{cases} \infty & R \le \sigma_{BB} \\ 0 & R > \sigma_{BB} \end{cases}$$
(2.2)

or LJ particles with interactions as in (2.1). Interaction parameters involving unlike species were obtained using conventional Lorentz-Berthelot mixing rules ⁶

$$\sigma_{AB} = \sigma_{BA} = (\sigma_{AA} + \sigma_{BB})/2 \tag{2.3}$$

$$\varepsilon_{AB} = \varepsilon_{BA} = (\varepsilon_{AA} \varepsilon_{BB})^{1/2}$$
(2.4)

The Percus Yevick (PY) equation for pure spherical particles has the form ⁷⁻¹⁰

$$y(\overline{R}_{1}, \overline{R}_{2}) = 1 + \rho \int_{V} y(\overline{R}_{1}, \overline{R}_{2}) f(\overline{R}_{1}, \overline{R}_{3})$$
$$\times [y(\overline{R}_{2}, \overline{R}_{3}) f(\overline{R}_{2}, \overline{R}_{3}) + y(\overline{R}_{2}, \overline{R}_{3}) - 1] dR_{3}$$
(2.5)

where f(R) is the Mayer function defined as

$$f(R) = \exp\left[-\beta U(R)\right] - 1 \tag{2.6}$$

and y(R) is defined as

$$y(R) = g(R) \exp[\beta U(R)]$$
(2.7)

A simpler and more useful form of this equation is obtained by transforming to bipolar coordinates

$$u = \left|\overline{R}_1 - \overline{R}_3\right|, \quad v = \left|\overline{R}_2 - \overline{R}_3\right|, \quad R = \left|\overline{R}_1 - \overline{R}_2\right|$$
(2.8)

In bipolar coordinates, the element of volume is expressed as

$$dR_3 = 2\pi u v \, du \, dv / R \tag{2.9}$$

and thus (2.5) can be transformed into

$$y(R) = 1 + 2\pi\rho R^{-1} \int_{0}^{\infty} y(u)f(u)u \, du \int_{|R-u|}^{R+u} [y(v)f(v) + y(v) - 1]v \, dv$$
(2.10)

For numerical purposes, it is convenient to transform again the *PY* equation (2.10) by defining the function 1,2,7,8

$$z(R) = y(R)R \tag{2.11}$$

Hence, an integral equation for z(R) can be obtained

$$z(R) = R + 2\pi\rho \int_{0}^{\infty} z(u)f(u) du \int_{|R-u|}^{R+u} [z(v)f(v) + z(v) - v] dv$$
(2.12)

For a binary mixture, equation (2.12) is generalized to

$$z_{\alpha\beta}(R) = R + \sum_{\gamma=A,B} 2\pi\rho_{\gamma} \int_{0}^{\infty} z_{\alpha\gamma}(u) f_{\alpha\gamma}(u) du \int_{|R-u|}^{R+u} [z_{\gamma\beta}(v) f_{\gamma\beta}(v) + z_{\gamma\beta}(v) - v] dv$$
(2.13)

where $\alpha\beta = AA$, AB, or BB. The numerical procedure used to solve the multi-component *PY* equation is similar to that used to solve the pure-fluid variant. One starts with

$$z_{\alpha\beta}(R) = R \tag{2.14}$$

for all four functions $z_{\alpha\beta}(R)$ and proceeds to solve the four integral equations (2.13) by iteration. [For more details, see references (1) and (2)]. Once the functions $z_{\alpha\beta}(R)$ are obtained, the pair correlation functions can be calculated using equations (2.7) and (2.11).

2.2 Monte Carlo simulations

Pair correlation functions were also calculated using Monte Carlo (*MC*) simulations in the canonical ensemble, that is at fixed *N* (number of particles), *V* (system volume), and *T* (temperature). For convenience, the quadratically shifted-force version of the Lennard-Jones interaction was used in the simulations.¹¹ The cutoff distance R_c was taken to be $2.5\sigma_{\alpha\beta}$ (where $\alpha\beta = AA$, *BB*, or *AB*). In all cases, a minimum of 300 particles was used. Since the simulations were performed in the canonical ensemble, only random trial displacements were employed. Cluster moves were not employed in the mixtures involving large size asymmetry. Instead, multiple independent simulations (a minimum of five in the case of large size asymmetry, and a minimum of three in other cases) were performed. The reported *PCF*s represent the mean of the independent runs. The standard deviation gives an indication of how well configuration space is explored. Each

simulation consisted of an equilibration period of at least 500,000,000 trial moves and a subsequent production period of at least 5 billion moves. Maximum trial displacements for each species were adjusted to yield an acceptance rate of 0.40. In addition, systems composed of 500 and 1000 particles were investigated to verify that system size effects were not important. Within the uncertainties, which are taken as the standard deviation of at least three independent runs, system size effects were negligible.

3. <u>Results from the Percus Yevick (PY) equations and the Monte</u> Carlo simulations

In this section, we present a sample of the results obtained from (a) solution of the *PY* equations and (b) by Monte Carlo simulations. We have carried out four sets of calculations for a mixture composition of $x_A = 0.1$ (where x_A is the solute mole fraction) and temperature T = 1. These are discussed in the following subsections:

3.1 <u>Dependence on the solvent size parameter</u>

The first series consists of results obtained for a fixed solute diameter $\sigma_{AA} = 1$ while varying the solvent diameter σ_{BB} . The other parameters for these calculations are

$$\varepsilon_{AA} / k_B T = \varepsilon_{BB} / k_B T = 1$$
, and $\eta = 0.4$ (3.1)

where η is the packing fraction, defined as

$$\eta = \frac{\pi}{6} \left(\rho_A \sigma_{AA}^3 + \rho_B \sigma_{BB}^3 \right) \quad . \tag{3.2}$$

where ρ_i is the number density of species *i*.

Figures 1 and 2 show the *PCF*'s calculated by *PY* equations for $\sigma_{BB} = 1$ to 5 and $\sigma_{BB} = 6$ to 10, respectively. Figure 3 shows $g_{AA}(R)$ in the region near the first maxima. As can be seen from these figures, the height of the first peak of g_{AA} increases with solvent size σ_{BB} while the heights of the first peaks of either g_{AB} and g_{BB} remain relatively constant. In Figure 4, the heights of the first and second peaks of the *PCF*'s predicted by theory and simulation are compared. The predictions of the two methods are in good agreement.

3.2 Dependence on packing fraction *n*

In this series of calculations, the packing fraction η is varied while fixing the following parameter values

$$\sigma_{AA} = 1, \qquad \sigma_{BB} = 6$$

$$\varepsilon_{AA} / k_B T = \varepsilon_{BB} / k_B T = 1 \qquad (3.3)$$

We vary η between 0.01 and 0.5. Figures 5 and 6 show the results computed by using the *PY* equations. In both the pure *LJ* liquid and LJ mixtures,^{1,2,12} it is well known that the first peak increases with increasing η . The interesting finding in our calculations is that the height of the first peak in g_{AB} almost does not change, while that of g_{BB} changes only slightly, with increasing η . In contrast, the height of the first peak in g_{AA} changes quite dramatically with η . Figure 6 shows the details of g_{AA} around the first maxima. Figure 7 compares the locations of the first and second peaks of the *PCF* obtained by the two methods.

3.3 Dependence on ε_{AA}

Figure 8 shows a series of results with the following fixed parameters

$$\sigma_{AA} = 1, \qquad \sigma_{BB} = 6$$

$$\varepsilon_{BB} / k_B T = 1, \qquad \eta = 0.4, \qquad (3.4)$$

while varying ε_{AA} . Note that in this case where $\varepsilon_{AA}=0$, the solute is treated as a hard sphere. Again, as expected, the solvent *PCF*, g_{BB} , does not change significantly, indicating that the solvent is not affected by the solute-solute interactions. On the other hand, g_{AA} changes considerably with ε_{AA} . A comparison of the peak heights predicted by the *PY* equations and *MC* simulation is provided in Figure 9.

3.4 Dependence on ε_{BB}

In the last series of calculations, the influence of the strength of solvent-solvent interaction is investigated. Other relevant parameter values were held fixed

$$\sigma_{AA} = \sigma_{BB} = 1 ,$$

$$\varepsilon_{AA} / k_B T = 0,$$

$$\eta = 0.4 \tag{3.5}$$

Notice that this corresponds physically to a hard-sphere solute in a LJ solvent. In the case where $\varepsilon_{BB} = 0$, the solvent is also a hard-sphere. The predictions of the *PY* equations are shown in Figure 10. Several important aspects of these results should be noted. First, the function g_{AB} is relatively insensitive to the strength of the solvent-solvent interaction. On the other hand, the function g_{BB} changes as expected for a normal liquid ¹⁰, i.e., all the peaks increase with ε_{BB} . These results are similar to the results obtained in one dimensional systems.^{3,3,14}

The most interesting finding is the behavior of g_{AA} . With increasing ε_{BB} , the height of the first peak of g_{AA} increases even more than the height of the first peak of g_{BB} . More important is the *range* of the solute-solute correlation, which grows with ε_{BB} .

Figure 11 shows the comparison with the *MC* results. We suspect that the disagreement between the two sets of results in this case is due to a phase separation. To clarify this point, we calculated the finite Kirkwood-Buff integrals defined by

$$G_{ij}(R_M) = \int_0^{R_M} [g_{ij}(R) - 1] 4\pi R^2 dR$$
(3.6)

Figure 12 shows that for small values of ε_{BB} , the function $G_{ij}(R_M)$ behaves "normally", i.e., as expected.¹⁰ However, for larger values of ε_{BB} the functions $G_{ij}(R_M)$ do not seem to converge as R_M increases. We also calculated the parameter

$$\Delta_{AB} = G_{AA} + G_{BB} - 2G_{AB} \tag{3.7}$$

Although we do not have the Kirkwood-Buff integrals (i.e., $G_{ij}(R_M \to \infty)$) the values of G_{ij} at $R_M = 10$ as well as Δ_{AB} , as reported in Table 1 indicates that something grows "wild" as we increase ε_{BB} . In Figure 13, we show a phase-separated configuration for $\varepsilon_{BB} = 1.1$.

4. <u>Discussion</u>

All the results reported in the previous sections in terms of the PCF may be reinterpreted in terms of the potential of mean force (PMF). The relationship between the two quantities is

$$W_{ii}(R) = -k_B T \ln g_{ii}(R) \tag{4.1}$$

Since we are interested in the solute-solute *PMF*, and since the direct solute-solute interaction is kept constant in each of the series of results, we can reinterpret the results in terms of the solvent induced interaction, i.e., we write

$$W_{AA} = U_{AA} + \delta A_{AA} \tag{4.2}$$

where U_{AA} is the direct solute-solute interaction and δA_{AA} is the solvent induced part of the *PMF*. The quantity δA_{AA} was studied extensively in connection with the problem of hydrophobic interactions.^{1,2}

There are several conclusions that can be drawn from the results of this work. The first is "technical"; that is the good agreement between the *PY* and the *MC* results proves once again the reliability of the *PY* equations. Even in the case where the results disagree, we can trace the origin of the discrepancy, and learn something about the applicability of the *PY* approximation in regions near phase separation.

The second conclusion is similar to the one drawn in a previous article (Ref. 3). As in reference 3, we found that in a one-dimensional system of mixtures that the correlation can be made large, or the solute-solute *PMF* can be made deeper by varying the solvent-solvent interactions. These findings strongly indicate that the solute-solute *PMF* for non-polar solutes in real water is basically a result of the *strength* of the solvent-solvent interactions. In real water, these interactions are due to hydrogen-bonding. However, it seems that hydrogen-bonding *per se*, or the peculiarities of the structure of water, are not necessary for the manifestation of strong solute-solute correlation, as is currently believed to be the case for so-called hydrophobic interactions.

As was also pointed out in reference 3, the extended *range* of the solute-solute *PCF* in a solvent with strong intermolecular interactions (or at low temperatures) is also not a phenomenon relevant to the hydrophobic interaction. In our case, it is probably due to the fact that the mixture becomes less symmetrical and less ideal, and perhaps approaching the region of phase separation.

The values of $O_{ij}(R_M = 10)$ and Δ_{AB} for the series of calculations in section 5.4				
	$\varepsilon_{BB} = 0$	$\varepsilon_{BB} = 0.5$	$\varepsilon_{BB} = 1.0$	$\varepsilon_{BB} = 1.5$
G _{AA}	-1.09	10.36	414.8	1843
G_{AB}	-1.09	-3.27	-84.17	-443
G _{BB}	-1.09	-0.67	15.53	105
Δ_{AB}	0	16.23	598.7	2834

Table 1 The values of $G_{ii}(R_M = 10)$ and Δ_{AB} for the series of calculations in section 3.4

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Figure captions

Figure 1: The pair correlation functions (*PCF*) for a mixture of a solute A in a solvent B predicted by the *PY* equations. The parameters for this series are provided in equations 3.1.

Figure 2: Same as in Figure 1 but for higher values of the solvent diameters $\sigma_{_{RB}}$.

Figure 3: The same as in Figure 1 and 2 but a close up view near the first peak of the *PCF*.

Figure 4: Comparison of the locations of the first and second peaks of g_{AA} obtained by solution of the Percus Yevick equations (diamonds) and by Monte-Carlo simulations (circles). Error bars represent the standard deviation of at least three independent runs.

Figure 5: Dependence of the *PCFs* on the packing fraction. Parameters for this series are provided in equations 3.3.

Figure 6: As in Figure 5, but a close up view near the first peak.

Figure 7: Comparison of the results from *PY* (diamonds) and *MC* (circles) for the first and second peak of g_{AA} and their dependence on η . Error bars represent the standard deviation of at least three independent runs.

Figure 8: Dependence of the *PCF* on the solute-solute energy parameter ε_{AA} . The other parameters for this series are provided in equations 3.4.

Figure 9: Comparison of the results from the *PY* (diamonds) and the *MC* (circles) for the first and second peaks of g_{AA} and the dependence on ε_{AA} . Error bars represent the standard deviation of at least three independent runs.

Figure 10: Dependence of the *PCF* on the solvent-solvent energy parameters ε_{BB} . The other parameters for this series are provided in equations 3.5.

Figure 11: Comparison of the results from the *PY* (diamonds) and *MC* (circles) for the first and second peaks of g_{AA} and their dependence on ε_{BB} . For clarity, the upper panel corresponds to the height of the first peak in g_{AA} , and the lower panel corresponds to the height of the second peak. Error bars represent the standard deviation of at least three independent runs.

Figure 12: The finite Kirkwood-Buff integrals for the same series as in Figure 10. The four columns correspond to the four values of $\varepsilon_{BB}(0,0.5,1.0,1.5)$ as in Figure 10. Figure 13: Phase separation for a hard-sphere solute in a LJ solvent ($\varepsilon_{BB} = 1.1$) observed in MC simulation. The total number of particles used in this simulation was 1000. (a) Both solvent and solute are shown. (b) For clarity, the solvent particles have been removed. Note also that periodic boundaries are applied.

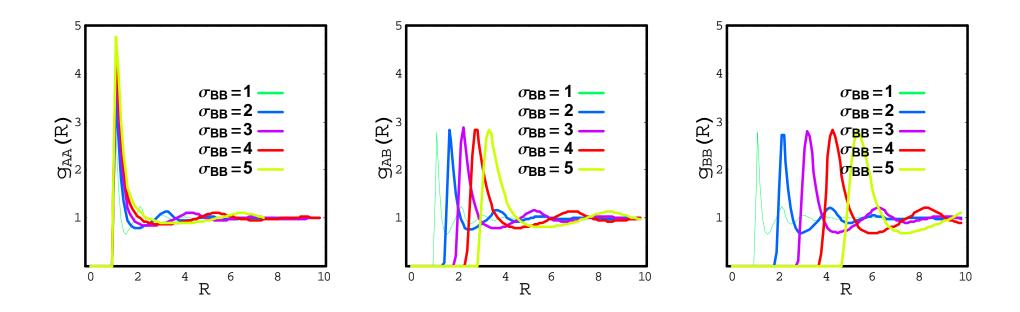


Figure 1

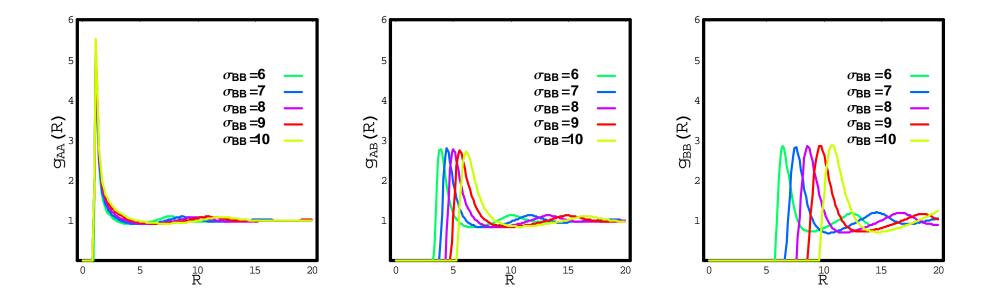
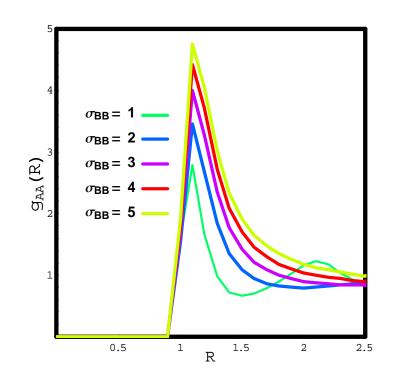


Figure 2



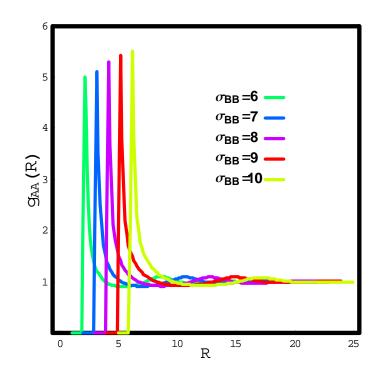


Figure 3

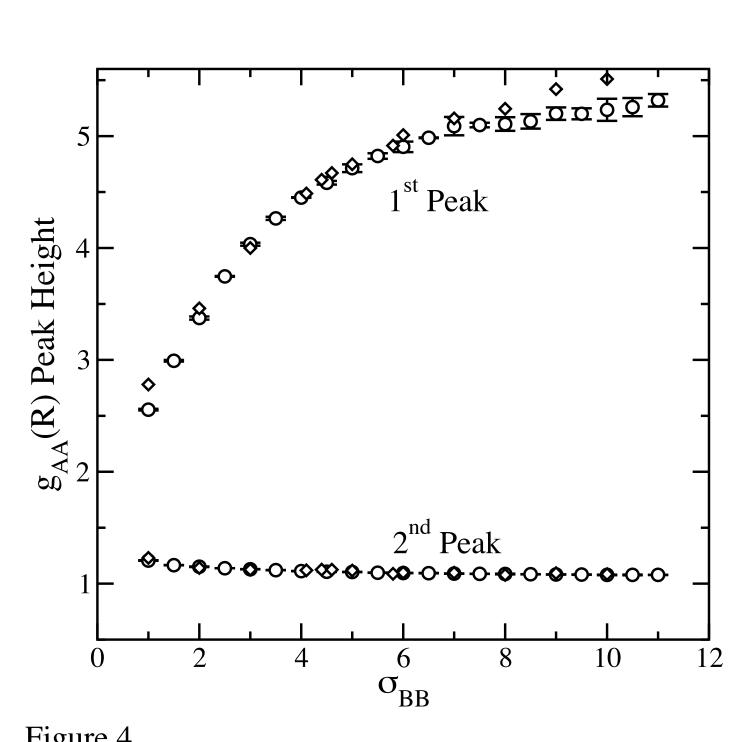
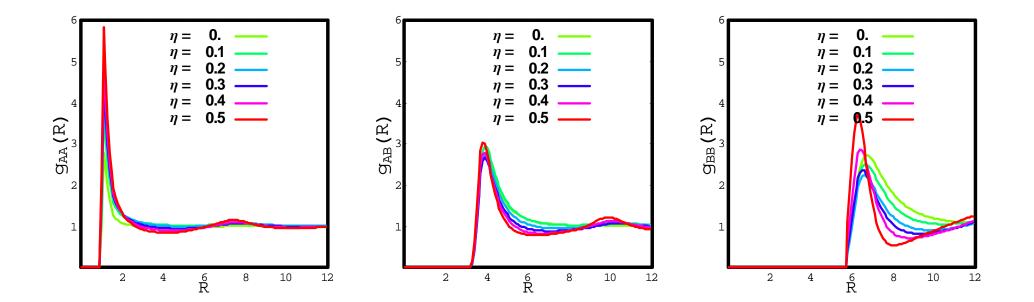
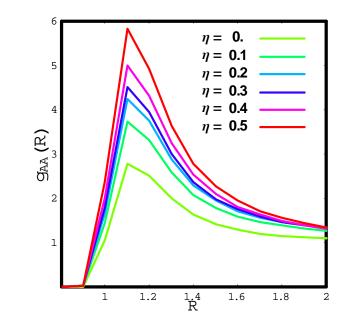


Figure 4





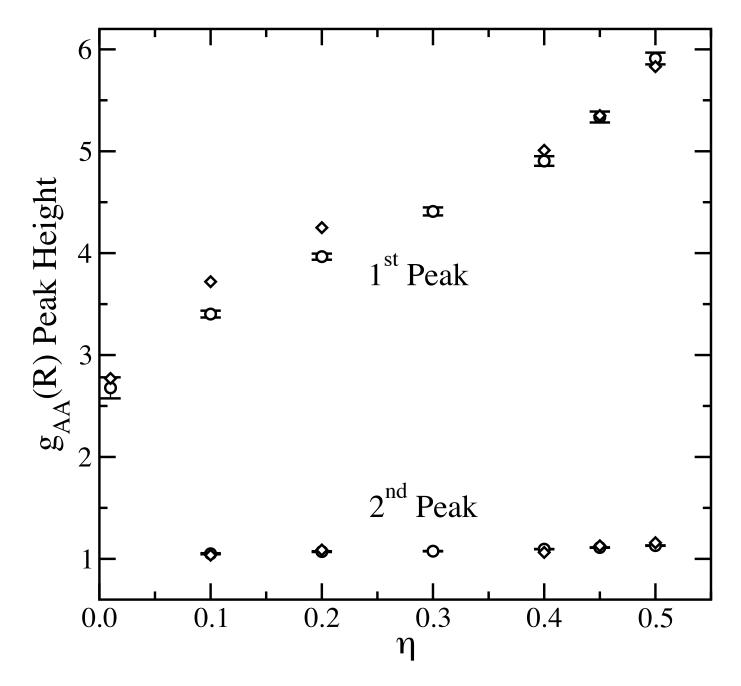


Figure 7

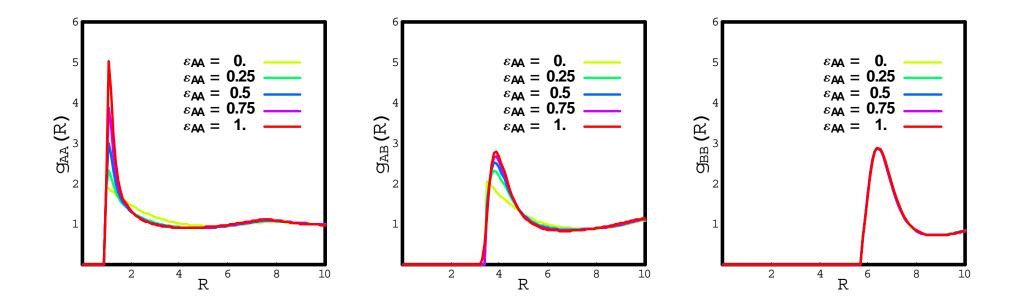


Figure 8

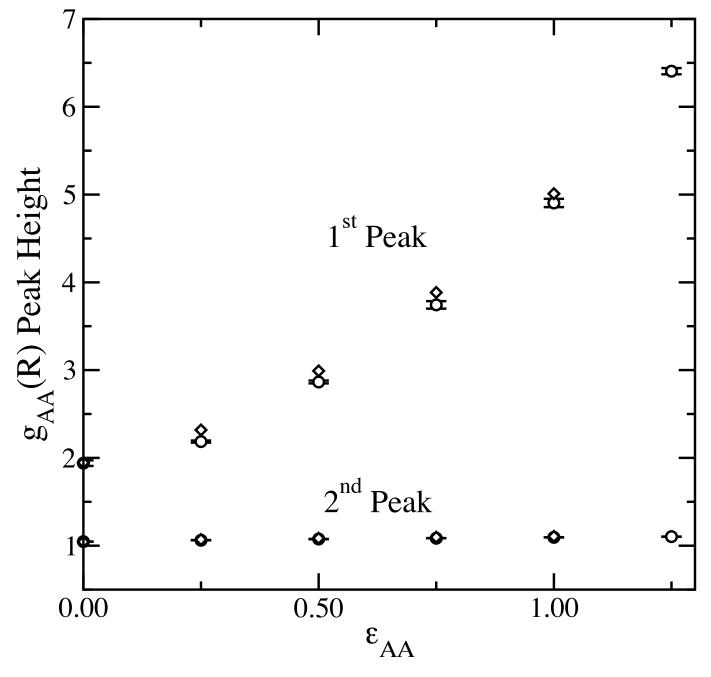


Figure 9

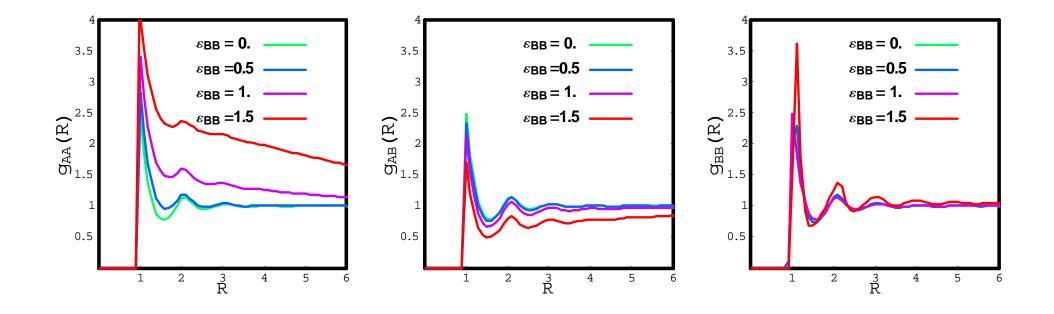


Figure 10

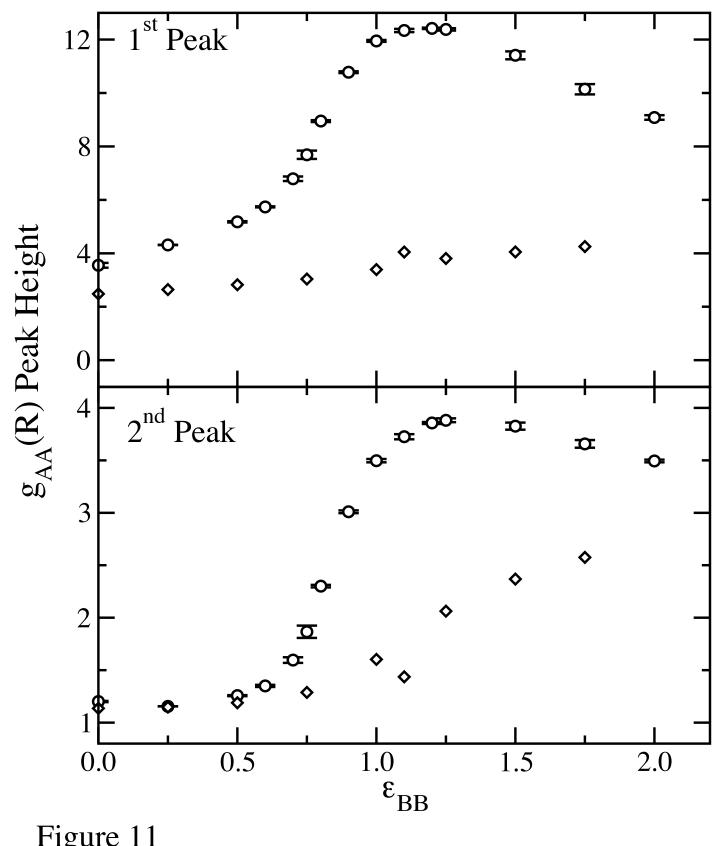
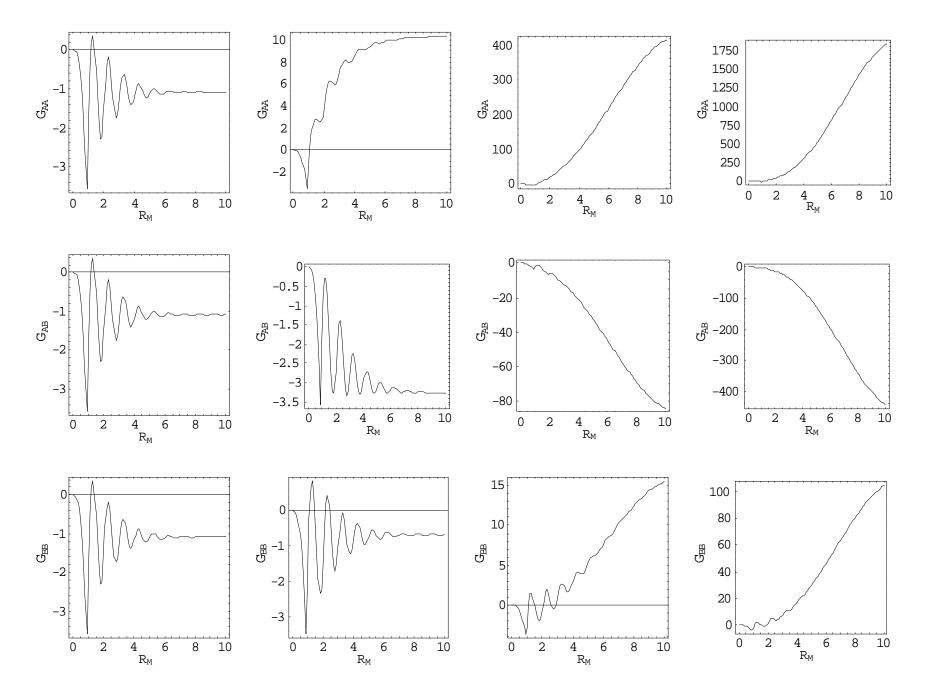


Figure 11



Fiaure 12

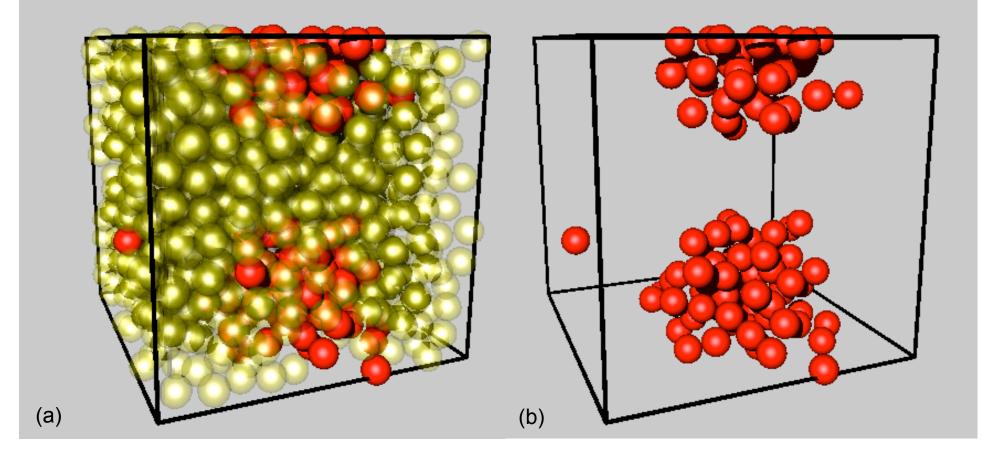


Figure 13.